

## TREATMENT OF DOMESTIC WASTEWATER IN SHALLOW WASTE STABILIZATION PONDS FOR AGRICULTURAL IRRIGATION REUSE

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### Abstract:

Waste stabilization ponds are a well established wastewater treatment system being considered by World Health Organization as one of the most appropriated technology for domestic wastewater when agricultural reuse is considered, especially in developing countries. This study was performed in a series of pilot-scale stabilization ponds, being one facultative and three maturation ponds, with depths varying from 0.44 to 0.57 m. The substrate to be treated was composed of a mixture of domestic wastewater and previously anaerobically treated leachate. The experimental system was monitored in two different phases, in which the hydraulic retention times were 15 (phase 1) and 10 days (phase 2). Termotolerant coliform removal efficiencies were 3.8 log<sub>10</sub> units in both phases while organic matter (BOD<sub>5</sub>) removal was 87 and 68% for phases 1 and 2, respectively.

**Keywords:** Wastewater treatment; agricultural reuse; shallow ponds

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## INTRODUCTION

Well designed and operated waste stabilization ponds (WSP) systems can satisfactorily remove undesired constituents from wastewater such as biodegradable organic matter, suspended solids and pathogenic microorganisms, besides to promote the retention of nutrients which favourably contributes to the use of such effluents in agricultural irrigation (Mara, 2001).

Such WSP are a well known technology for the treatment of domestic wastewater and is considered by the World Health Organization (WHO) as the most appropriated means of wastewater treatment when agricultural reuse is considered (WHO, 1989) specially for developing countries, due to its construction, operation and maintenance low costs (Arthur, 1983). Research developed by Silva (1982) has shown the high degree of treatment reached by the effluent of waste stabilization ponds, both in terms of organic matter and pathogenic microorganisms. The high hydraulic retention times (HRT), which are common in WSP systems, in conjunction with adverse factors to microorganisms, are the main cause of the high bacteriological quality effluent, which have also the characteristic of presenting high level of nutrients, being therefore, suitable for agricultural irrigation (Mara, 1996).

According to Arthur (1983), WSP are the most suitable wastewater treatment option for developing countries located in tropical or subtropical regions, where generally land is available and cheap and climate is favourable for the treatment process. The idea of reusing treated wastewater has been developing to be part of the rational use of water resources, besides being an important practice in arid and semi-arid areas (Shilton, 2005), such as northeastern Brazil.

In Brazil, the indirect and uncontrolled reuse of wastewater is a routine practice. This activity is more evident in semi-arid areas in northeastern Brazil, where

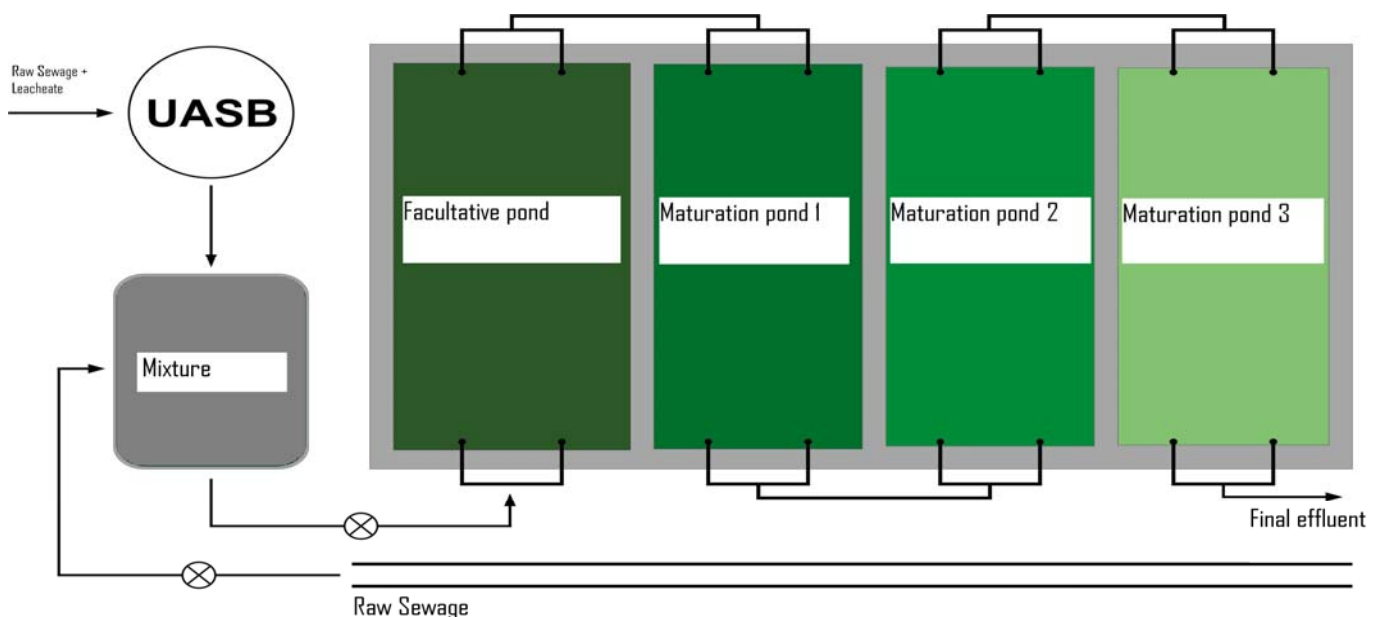
the lack of wastewater treatment is rapidly negatively affecting the water resources. On the other hand, this region of Brazil, due to its geographic and economical characteristics, has favourable conditions for the wastewater reuse and leads small and medium farmers to use a non conventional water to replace the lack of water for irrigation. Furthermore, the wastewater reuse presents other advantages, such as: water pollution control, water and fertilizers savings, recycle of nutrients and the increase in agricultural production (Athayde Júnior, 1999).

In this context, the objective of this paper is to evaluate the performance of a series of shallow WSP treating domestic wastewater for the production of an effluent suitable for agricultural irrigation according to legal aspects.

## MATERIAL AND METHODS

The research was conducted in Estação Experimental de Tratamentos Biológicos de Esgotos Sanitários – EXTRABES, located in Campina Grande – PB, Brazil.

The experimental system comprised four ponds, in which the first is a facultative one and the other three are maturation ponds. The series of WSP were preceded by a UASB which received a mixture of raw sewage (98%) and leachate (2%). The UASB effluent (80%) was mixed with raw sewage (20%) before going to the WSP series. These mixture percentages were used in both experimental phases. **Figure 1** schematically shows the pond system, while **Table 1** shows the operational features. The parameters analyzed were pH, COD, BOD<sub>5</sub>, thermotolerant coliform, total solids, volatile total solids, suspended solids, volatile suspended solids, total alkalinity, volatile acids, ammonia, nitrate, total phosphorus, soluble orthophosphate.



**Fig.1** Scheme of experimental WSP system.

**Table 1.** Physical and operational features of the WSP system

Pond	Width (m)	Length (m)	Depth (m)	Surface area (m <sup>2</sup> )	Volume (m <sup>3</sup> )	HRT (days)	
						Phase 1	Phase 2
Facultative	1.00	2.05	0.57	2.05	1.17	4.7	3.1
Maturation 1	0.88	2.04	0.53	1.79	0.95	3.8	2.5
Maturation 2	0.88	2.01	0.48	1.76	0.84	3.4	2.3
Maturation 3	0.89	2.00	0.44	1.78	0.78	3.1	2.1

Physicochemical and microbiological analyses were performed in accordance with APHA *et al.* (1995), with exception for chlorophyll *a*, which was determined according to Jones (1979) and sampling occurred weekly during five and four months in phase 1 and 2.

## RESULTS

**Table 2** shows the results for the characterization of the substrate from the mixture tank, while **Table 3** shows the results for the final effluent (maturation pond 3), both for phase 1.

Analyzing data from **Table 2**, it can be noticed that the substrate used to feed the WSP system presented good conditions for biological treatment, since pH values were around 7.8, with high alkalinity values and low volatile acids concentration. BOD<sub>5</sub> varied from 126 to 262 mg/L while mean value for total solids was 1422 mg/L. BOD<sub>5</sub>/COD ratio was 0.41, indicating some biodegradable material. Thermotolerant coliform numbers were around 10<sup>6</sup> CFU/100 mL.

**Table 3** shows the final effluent quality in phase 1. This effluent was alkaline, with maximum pH of 9.4, due to the photosynthetic activity of algae, which were characterized by chlorophyll *a* values of up to 678 µg/L. BOD<sub>5</sub> removal efficiency was 89%, with final effluent concentration of 20 mg/L. For thermotolerant coliform, the removal efficiency was 3.8 log<sub>10</sub> units what indicates a possible high reduction for pathogenic microorganisms and the good microbiological quality of the final effluent. Thermotolerant coliform removal in waste stabilization ponds is generally associated with high pH and dissolved oxygen levels and HRT (Athayde Júnior *et al.*, 2000) as occurred in this present study. In phase 1, mean ammonia removal was 90%. Since the

ponds herein considered were very shallow, the ammonia removal is associated with volatilization and biological assimilation by algae (Athayde Júnior *et al.*, 2000). With regards to phosphorus, in phase 1 the removal percentage was 61.6%. This removal is generally associated with chemical precipitation in high pH levels and subsequent biological assimilation by algae (Athayde Júnior *et al.*, 2000). Total solids concentration in the final effluent was 1207 mg/L in phase 1. This high level of solids is associated with the growth of algae and poses no risk for the soil salinization (Ayers & Westcot, 1985; Mara, 1996).

Therefore, in general, the effluent of the pond series, operated with 15 days of HRT, presented an effluent suitable for irrigation, resulting in several benefits such as economical, social and environmental ones.

**Table 4** shows the final effluent quality in phase 2. In general, in comparison to the substrate of phase 1, the substrate in phase 2 presented lower levels of parameters concentration. BOD<sub>5</sub>/COD ratio was 0.36 (as compared to 0.41 in phase 1).

**Table 5** shows the final effluent quality in phase 2. The BOD<sub>5</sub> removal efficiency was 68% in comparison to 89% in phase 1. Suspended solids also presented lower removal efficiency in phase 2. These lower removal efficiencies may be associated with the lower BOD<sub>5</sub>/COD ratio in phase 2. For thermotolerant coliform, the removal was of 3.8 log<sub>10</sub> units, which was the same as in phase 1, resulting in less than 10<sup>3</sup> CFU/100 mL with a cumulative HRT of 10 days. Ammonia and phosphorus removal were 82.5% and 8%, respectively, in phase 2. In fact, this low removal for phosphorus is desirable, since this nutrient does not presents toxicity in agriculture.

**Table 2.** Mixture tank substrate characterization – phase 1

Parameter	Unit	<i>n</i>	minimum	maximum	mean <sup>1</sup>
pH	-	18	7.7	8.1	7.8
Total alkalinity	mgCaCO <sub>3</sub> /L	18	282	980	642
Volatile acids	mgH <sub>Ac</sub> /L	18	34	110	72
BOD <sub>5</sub>	mg/L	16	126	262	183
COD	mg/L	17	304	661	445
Total solids	mg/L	18	1 007	2 114	1 422
Volatile total solids	mg/L	18	208	1 144	398
Suspended solids	mg/L	18	92	196	141
Volatile suspended solids	mg/L	14	83	167	118
Ammonia	mg/L	18	29	117	77
Total phosphorus	mg/L	16	5.7	18.2	12.0
Soluble orthophosphate	mg/L	16	3.4	11.2	7.0
Thermotolerant coliform	CFU/100mL	18	1.8×10 <sup>6</sup>	2.4×10 <sup>7</sup>	6.5×10 <sup>6</sup>

<sup>1</sup>Arithmetic mean for all the parameter except for thermotolerant coliform, which was used the geometric mean.

**Table 3.** Physicochemical and microbiological characterization of final effluent – phase 1

Parameter	Unit	<i>n</i>	minimum	maximum	mean
pH	—	18	7.8	9.4	8.6
Total alkalinity	mgCaCO <sub>3</sub> /L	18	236	629	407
Volatile acids	mgH <sub>Ac</sub> /L	18	13	32	22
BOD <sub>5</sub>	mg/L	16	2.7	34.0	20.1
COD	mg/L	17	61	615	208
Total solids	mg/L	18	788	1998	1207
Volatile total solids	mg/L	18	68	843	202
Suspended solids	mg/L	18	20	109	49
Volatile suspended solids	mg/L	14	2	95	38
Ammonia	mg/L	18	1.7	22.0	7.8
Total phosphorus	g/L	16	2.5	9.1	4.6
Soluble orthophosphate	mg/L	16	2.0	6.2	3.6
Thermotolerant coliform	CFU/100mL	18	130	6.6×10 <sup>3</sup>	1.0×10 <sup>3</sup>
Chlorophyll <i>a</i>	µg/L	18	71	678	263

<sup>1</sup>Arithmetic mean for all the parameter except for thermotolerant coliform, which was used the geometric mean.

**Table 4.** Mixture tank substrate characterization – phase 2

Parameter	Unit	<i>n</i>	minimum	maximum	mean
pH	—	18	7.7	8.5	8.0
Total alkalinity	mgCaCO <sub>3</sub> /L	18	264	392	329
Volatile acids	mgH <sub>Ac</sub> /L	18	7	56	24
BOD <sub>5</sub>	mg/L	18	13	73	44
COD	mg/L	18	42	203	149
Total solids	mg/L	14	614	767	708
Volatile total solids	mg/L	14	50	137	92
Suspended solids	mg/L	14	41	106	68
Volatile suspended solids	mg/L	14	34	88	57
Ammonia	mg/L	18	14.3	73.3	41.7
Total phosphorus	mg/L	16	1.1	10.2	5.0
Soluble orthophosphate	mg/L	16	3.1	4.8	3.8
Thermotolerant coliform	CFU/100ml	18	6.0×10 <sup>4</sup>	7.5×10 <sup>6</sup>	2.2×10 <sup>6</sup>

<sup>1</sup>Arithmetic mean for all the parameter except for thermotolerant coliform, which was used the geometric mean.

**Table 5.** Physicochemical and microbiological characterization of final effluent – phase 2.

Parameter	Unit	<i>n</i>	minimum	maximum	mean
pH	—	18	8.1	9.3	8.7
Total alkalinity	mgCaCO <sub>3</sub> /L	18	194	284	237
Volatile acids	mgH <sub>Ac</sub> /L	18	8	20	13
BOD <sub>5</sub>	mg/L	18	3	27	14
COD	mg/L	18	15	285	120
Total solids	mg/L	14	636	777	713
Volatile total solids	mg/L	14	12	74	37
Suspended solids	mg/L	14	11	69	32
Ammonia	mg/L	18	2.6	15.0	7.3
Total phosphorus	mg/L	16	1.1	7.5	4.6
Soluble orthophosphate	mg/L	16	1.4	7.2	3.8
Thermotolerant coliform	UFC/100mL	18	22	3.1×10 <sup>3</sup>	3.7×10 <sup>2</sup>
Chlorophyll <i>a</i>	µg/L	17	74.6	1 215.8	271.0

<sup>1</sup>Arithmetic mean for all the parameter except for thermotolerant coliform, which was used the geometric mean.

## CONCLUSION

Waste stabilization ponds showed to be suitable for the combined treatment of leachate and domestic wastewater. The series of shallow ponds showed to be very efficient in terms of thermotolerant coliform removal, being needed about 10 of HRT for the effluent

to reach the treatment level which is considered suitable for the reuse in irrigation. The substrate BOD<sub>5</sub>/COD ratio and the HRT poses influence on the treatment efficiency. Furthermore, the nutrient level found in the final effluent is another aspect which is favourable for the reuse in agricultural irrigation, resulting in water conservation.

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